What is claimed is:

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- 1. Lubricant base oil consisting essentially of a normal paraffin and an isoparaffin, and satisfying the following requirements (a) and (b):
- (a) an average carbon number Nc in one molecule is not less than 28 but not more than 40; and
- (b) an average branch number Nb in one molecule, which is derived from a ratio of CH<sub>3</sub> carbon to total carbon determined by <sup>13</sup>C-NMR analysis and the average carbon number Nc in one molecule is not more than (0.2Nc 3.1) but not less than 1.5.
- 2. Lubricant base oil according to claim 1, which is obtained from an isomerization of a starting straight-chain hydrocarbon material having an average carbon number Nc in one molecule of not less than 25.
  - 3. Lubricant base oil according to claim 2, wherein the starting straight-chain hydrocarbon material is a Fischer-Tropsch synthetic wax.
- 4. A method of producing lubricant base oil according to claim 3, which comprises subjecting starting oil composed of a Fischer-Tropsch synthetic wax having a 10% distillation temperature of not lower than 360°C to an isomerization under a condition that a decreasing ratio of a fraction having a boiling point of not lower than 360°C is not more than 40% by weight.
  - 5. A method of producing lubricant base oil according to any one of claims 1 to 3, which comprises the following steps:
  - (1) hydroisomerizing a starting straight-chain hydrocarbon material in a first reactor;
  - (2) separating oil obtained by the hydroisomerization into a fraction mainly composed of a normal paraffin (fraction  $\alpha$ ) and a fraction mainly composed of an isoparaffin (fraction  $\beta$ );
    - (3) hydroisomerizing the fraction  $\alpha$  in a second reactor, and mixing oil obtained from the hydroisomerization (fraction  $\gamma$ ) with the fraction  $\beta$ .
  - 6. A method according to claim 5, wherein the hydroisomerization in the second reactor is carried out under a reaction condition that a decreasing ratio of a fraction having a boiling point of not lower than 360°C in the hydroisomerization at the second reactor is lower than a

decreasing ratio of a fraction having a boiling point of not lower than 360°C in the hydroisomerization at the first reactor.

- 7. A method according to claim 5, wherein the starting straightchain hydrocarbon material is a Fischer-Tropsch synthetic wax.
- 8. A method according to claim 7, wherein the Fischer-Tropsch synthetic wax has an average carbon number Nc of not less than 25.

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9. A method according to claim 5, wherein the hydroisomerization in the first reactor is carried out under a reaction condition that a decreasing ratio of a fraction having a boiling point of not lower than 360°C is not more than 50% by weight.